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### Method for controlling the temperature of a cellulosic web entering a dryer

The present invention relates to a method for controlling the temperature of a web, which is formed from cellulosic pulp and is to be passed to a dryer, by way of applying 5 temperature-controlled liquid to the web.

Conventionally, a traveling cellulosic web has been heated by flooding the web with a liquid, whereby uncontrollable penetration of the liquid into the web occurs. As this overflow-flooding step of heating takes place in an open space, it is hampered by 10 problems from the overflow of the liquid and release of expansion steams.

It is an object of the present invention to overcome the above-mentioned problems by virtue of a method characterized by a step of passing the formed web into a closed space defined by two wires and side deckles, wherein temperature-controlled liquid 15 is applied at controlled pressure and flow rate through the wire into the web.

Generally, the closed spaced remaining between the wires is maintained at a moderate positive pressure. The method according to the invention is capable of controllably setting the web temperature at a desired level, e.g., close to 100 °C, thus 20 improving water removal from the web in the press section next downstream of the closed space, whereby the web is maximally hot and has a high solids content at the instant the web enters the dryer section. Furthermore, the method according to the invention may be applied generally in the temperature control of a web, even for cooling, thus making it possible to set the web temperature optimally for drying a 25 cellulosic web. The method also facilitates addition of chemicals into the web in order to improve the qualities of the web.

According to the invention, the liquid can be applied advantageously via a box to the web, either from the underside of the lower wire or from the top side of the upper 30 wire or, alternatively, from both sides either simultaneously or alternatingly. The penetration of the liquid being applied into the web may be improved if so desired by way of maintaining a pressure difference between the liquid application point and the

side of the web opposite to the application point. This arrangement can be accomplished using, e.g., suction boxes that are located on the opposite side of the web relative to the liquid application point, substantially aligned with said point.

5 There may be located a plurality of liquid feed points above or below the web or in alternating positions both above and below the web.

As the web enters the closed space between the wires, its solids content is in a range of about 0.5 % to about 4.0 %, while the solids content is in a range of about 20 % to 10 about 30 % when the web exits the closed space and enters the press section.

In the following, the invention will be described in greater detail by making reference to the appended drawing showing a schematic side elevation view of an apparatus layout suitable for implementing the method according to the invention.

15 The method employs a twin-wire machine having a bottom wire 1 and top wire 2. Cellulosic pulp is fed into the headbox 3 of the twin-wire machine, wherefrom the pulp flows as a uniform sheet into a closed space 4 defined by the bottom wire 1 and the top wire 2 in cooperation with side deckles (not shown), wherein a web 5 is formed. When entering this closed space 4, the solids content of the web is typically 20 in a range of about 0.5 % to about 4.0 %. This closed space 4 is generally maintained at a moderate positive pressure.

25 In order to control the temperature of the web 5 to a desired level, below the bottom wire 1 and/or above the top wire 2 are placed liquid feed points 6, 7, 10 wherefrom to the web 5 is applied a liquid advantageously via a box at a controlled temperature, pressure and flow rate. As shown in the drawing, the liquid is applied to the web 5 first from below the bottom wire 1 at liquid feed points 6 and 10, whereupon liquid application takes place from above the top wire 2 at liquid feed points 7. Obviously, 30 the apparatus may incorporate more liquid feed points either above or below the web or in alternating positions both above and below the web.

When necessary, the penetration of the liquid being applied into the web 5 can be improved by means of suction boxes 8, 9 adapted to operate opposite to some or each one of the liquid feed points 6, 7, 10, substantially aligned with the opposed liquid feed point.

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According to an embodiment of the invention, the web is heated in the method of the invention to a temperature close to 100 °, whereby the removal of water from the web 5 is enhanced in the press section located downstream of the twin-wire region. Resultingly, the temperature and solids content of the web are elevated maximally 10 high as the web enters the dryer section, whereby drying of the web is speeded up and energy consumption of the dryer is lowered.

Alternatively, the method may also be employed for cooling the web 5 in order to set the temperature of the web 5 to an optimal level for drying a cellulosic web.

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Furthermore, the method according to the invention facilitates the addition of web quality improving chemicals into the web in conjunction with the liquid being applied to the web, thus allowing the control of, e.g., the pH of the web.

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When exiting the closed space 4 defined by the wires 1, 2, the solids content of the web has increased reaching from about 20 % to about 30 %.

## Claims:

1. A method for controlling the temperature of a web (5), which is formed from cellulosic pulp and is to be passed to a dryer, by way of applying temperature-controlled liquid to the web, **characterized** in that the thus formed web (5) is passed into a closed space (4) defined by two wires (1, 2) and side deckles, wherein temperature-controlled liquid (6, 7, 10) is applied at controlled pressure and flow rate through the wire (1, 2) to the web (5).
- 10 2. Method according to claim 1, **characterized** in that in the closed space (4) between the wires (1, 2) a moderate positive pressure is maintained.
3. Method according to claim 1, **characterized** in that liquid (6, 10; 7) is applied to the web (5) from below the bottom wire (1) and/or from above the top wire (2).
- 15 4. Method according to claim 3, **characterized** in that the penetration of the liquid being applied into the web (5) is improved by maintaining a pressure difference between the opposite sides of the web.
- 20 5. Method according to any of the previous claims, **characterized** in that the temperature of the web (5) is elevated substantially close to 100 °C.
6. Method according to any of the previous claims 4 - 5, **characterized** in that, in order to establish said pressure difference, a suction box (8, 9) is adapted to operate opposite to some or each one of said liquid feed points (6, 7, 10) on the other side of the web, substantially aligned with said liquid feed point.
- 25 7. Method according to any of the previous claims, **characterized** in that chemicals are added to the web (5) in conjunction with the liquid application in order to improve the qualities of the web.

8. Method according to claim 7, **characterized** in that the liquid application to the web (5) is adapted to take place at several successive points (6, 10; 7).

5        9. Method according to claim 8, **characterized** in that the liquid is applied alternately from above and from below the web.

10. Method according to any of the foregoing claims, **characterized** in that the solids content of the ingoing web (5) is about 0.5 - 4.0 % and the solids of the outgoing web prior to its entry into the dryer is about 20 - 30 %.